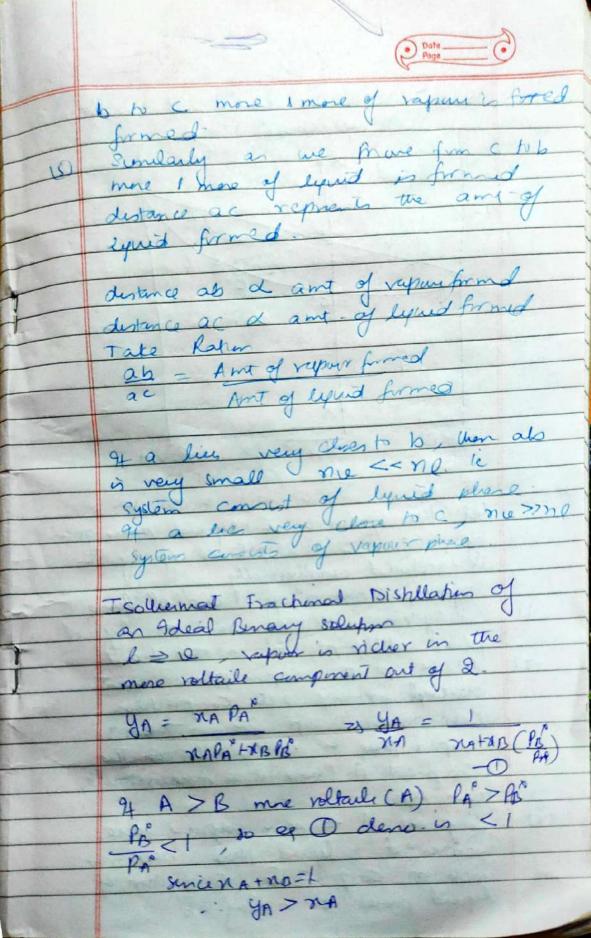


The upper curve is called lyudies curie & above this curve only liquid exist & below curve's called verpourous curve & only rapour enest. A pt in between the curves represent the system in which lyund I vapour coeres in equilibrium for a particular composition, the points on liquides & rapouns curves represent max. I min prenise, within which I phase can enist in epuebrium with each other It Posptem > pmax lquid eclos Paylor < prien vapour exist Prox > Prylim > Prien lyuid = rapery PB repur XA XA YA Ruse of It component A. composition is to be determined in liquid trapur ther a horizontal line is drawn Known as the tre line to the lyudus Srapurs Currl

Since A is chosen as the descubery variable then intersection of a vertical line from xx with liquides curve iè pt. b gives are value of p. & hon zontal line from Pe cultury the vapourous curve c gives vapour composition you is Lever Rule A point wither the liquid I raper phases shows I = v in equipmen from pt 'a! the amount: fraction of the constituent Am the lipid is given by pt-b rapus phase is given by Tie lin be reprents we ampost Of liquid , rapum pheres MA 1 yA Difference is only in the relative amounts of the phase from pt. to pt. (1) 9+ 'a' councides with b wat me ain rapour his just slaved from many The a' concide out of fraction you last drip of lywid place is left with ant fraction of not going to be converted into rappin phase 3) If we more from b' to compe s more of liquid phase changes to rapher phase.

Distance ba ocprents and of rapin formed since as we more from





When Prenue is reduced sollesmale 1cmp const verpu Pure B Let the system is in liquid prace gren by point a s pressure of system is reduced isothermally. system mores along a a a lene I system will remain in lyud phase the pt b' is reached (2) At the pt b, rapon phase just corresponds to p. "c" The vapour phase is more rich in the Comprest A (since it is more voltable Compred 1 is sero vapara are rich in component B, composition of liquid preses much along bb



If report ration is to be continued, we pressure of the system must be lowered. The overall state will more along the same vertical line by pt. a. At the pt a', the composition of lyvid I rapino phases is given by b' & c' respectively the relative of amounts of two phases is given by lever rule

Amount in liquid phase = dc'

Amount in rupun place a'b 94 l'is Justine reducid s wen the pt (" Justine there is negligible have of lyvid b" is left & vapour phone. In same as word of starting lyvid (7) As Pin further reduced & phase System is conveiled into one phase system consistent of rapour Procedure of 950thermal Frachenal removed & condensed separately the new equid composed is richer in more jo Haule Consphents; Vapour which are formed will be richer in

Still richer in more to Haile comprised
It this removing of superior from
Solution I condensing the responsed
several typic, there a stage
is reactived when respons consists
of only one of the more
rotable constructs a liquid that
of less rotable comprised
ceperation of constituents is
achieved

Jemperature Composition Diagram

of Benary Lywid Coledin

Def B. Pl. Normal B. pt

A reguired which has a higher V.P.

will have lover B.pt. Since len

heating is required to attain V.P.=

external hence.

A reguired with lower V. P. will

have high B. pt
B.pt of a Colubin have a

definite relation with the

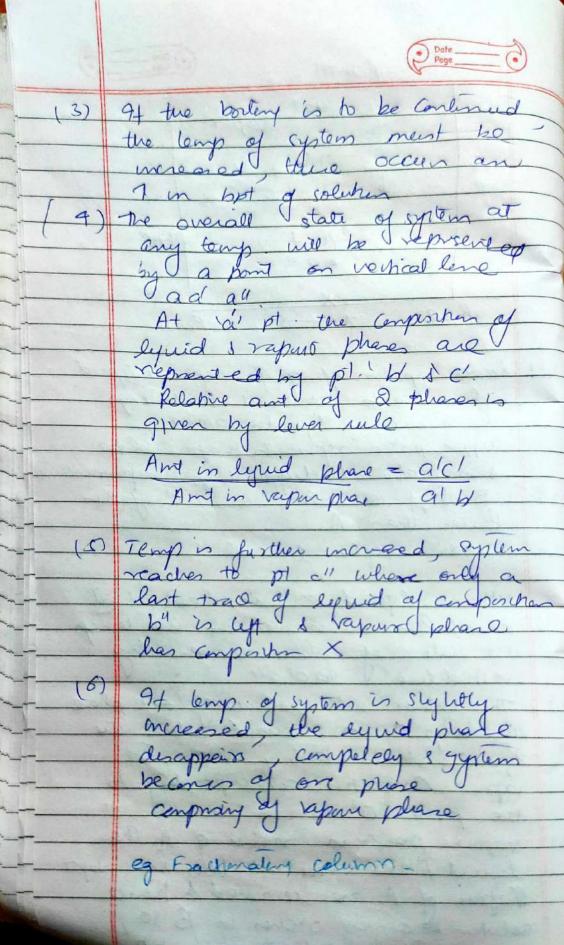
Composition of the Solution

So the anaph between Temple

Composition will be vereine

d prenons graph I no

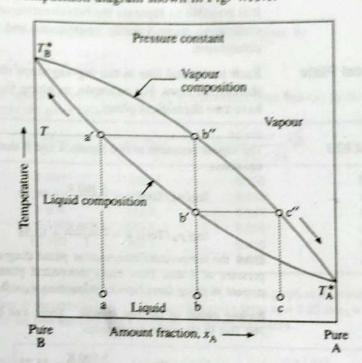
Pconst lyund TAX Pares Puret dower portion of graph represent liqued please as its stable at lower temps lover curve's lyude and upper portion reprients rapor place Bipt of B > A ie V. P of Bis 12) luces than A. Central region 1 = 0 (3) When a liquid mix is heated at const! P. on moreasing the length the state of system meres along verticalline aday The system will remain of one phase (1) till leslys I is scalled where the lyvid starts boiling with the Vapor Composition corresponding to the point C (2) vapors phase is vider of A than lyuid phase snece A was lover by Napon of A are removed & hence solution be comes victies in B 80



# 4.13 ISOBARIC FRACTIONAL DISTILLATION OF AN IDEAL BINARY SOLUTION

#### Underlying Principle

The isobaric process of distillation in which the external pressure is kept constant instead of temperature is more convenient and is often employed for the separation of constituents of a binary liquid system. The principle of separation of constituents using the isobaric fractional distillation may be explained with the help of temperature-composition diagram shown in Fig. 4.13.1.



g. 4.13.1 Principle of obaric distillation

- Let the starting composition of the solution to be distilled be represented by the point a. Let the temperature of the solution be raised till it starts boiling. At this stage, the vapour pressure of the solution is equal to the external pressure, which is kept constant throughout the distillation process. Usually the atmospheric pressure of 1 atm is employed for this purpose. The vapour which appeared at the boiling point T is represented by b". Since the latter is richer in the constituent A (the more volatile constituent), the residual liquid will become richer in the constituent B and will boil at a slightly higher temperature.
- Let the vapour formed at T be removed and condensed separately to yield distillate b. Let this new distillate be heated till it starts boiling. the vapour which now emerges is represented by c" and is still richer in the constituent A.
- If the above sequence of collecting the vapour, condensing them to give a new distillate and heating the new distillate to its boiling point is repeated several times, the vapour will continue to contain more and more of the constituent A and ultimately a stage would be reached where it would contain only this constituent.

The residual liquid at any stage can be mixed with the previous residual liquid and can be treated in the same way. The residual liquid continues to contain lesser and lesser of the more volatile constituent and thus more and more of the lesser volatile constituent. When the process is repeated several times, a stage would be reached when the residual liquid would contain only the lesser volatile constituent.

Thus, we see that by carrying out the above fractional distillation process, it is possible to separate the two constituents of a binary liquid mixture; vapour containing more volatile constituent and the liquid containing less volatile constituent.

### Theoretical Plate

Each horizontal line in the zig-zag steps shown in Fig. 4.13.1 is known as the theoretical plate. For example, in going from liquid of composition a to c, we have two theoretical plates.

## e Fractionating Jumn

The process of fractional distillation is extremely tedious and involves more time and labour as the separation is carried out in batches and in a discontinuous manner. However, these difficulties can be overcome by employing a fractionating

column, which essentially carries the distillation in a continuous manner. Figure 4.13.3 displays one such column commonly employed in industry. This is known as the bubble-cap column. It consists of a long tube carrying a large number of bubble-cap plates and is attached to a boiler at the bottom and to a condenser at the top. Each plate can hold a thin layer of liquid and has an overflow mechanism through which the excess liquid can pass to the plate just below it. It also has many bubble-caps through which the vapour passes upward after bubbling through the liquid. There is a temperature gradient along the length of the column, the top being cooler than the bottom. The various plates are thus situated at different temperatures and also hold the liquid at that temperature.

## Principle Underlying Fractionating Column

The principle of bubble-cap column can be illustrated very nicely with the help of temperature-composition diagram (Fig. 4.13.4).

Let the liquid be boiled at the bottom, say at temperature  $T_0$ . The vapour issuing has composition  $v_0$ . When this vapour is passed through the first plate, it is cooled to temperature  $T_1$  and thus its state is moved to the point a. At this state, some of the vapour condenses to form liquid of composition  $l_1$  and the

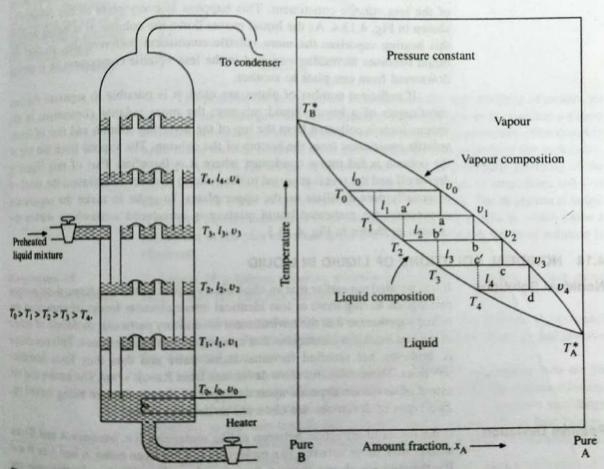


Fig. 4.13.3 Bubble-cap distilling column

Fig. 4.13.4 Scheme of redistribution of constituents in the distilling column

remaining vapour has composition  $v_1$ . The liquid formed contains  $more\ of\ the$  less volatile constituent. Next, the vapour of composition  $v_1$  is passed through the second plate whose temperature is  $T_2(T_2 < T_1)$ . Here the vapour is  $cooled\ to\ T_2$  and thus the state of system is moved from  $v_1$  to b. At this state, again part of the vapour is condensed to give liquid of composition  $l_2$  and the remaining vapour has composition  $v_2$ . Now the vapour has become more enriched in the more volatile constituent. This happens at every plate of the column as is also shown in Fig. 4.13.4. As the vapour moves up the column, it is being cooled; this cooling condenses the less volatile component preferentially, so that the vapour becomes increasingly enriched in the more volatile component as it passes upward from one plate to another.

Similarly, as the liquid flows down, its temperature is increased and again there is a redistribution of the constituents. For example, the liquid of composition  $l_3$  has flown from the plate 3 to plate 2. The liquid has been heated from  $T_3$  to  $T_2$  and thus the state of the system has moved from  $l_3$  to b'. Thus part of the liquid vaporizes to yield vapour of composition  $v_2$  containing more of the more volatile constituent. The resultant liquid has a composition of  $l_2$  and thus contains more of the less volatile constituent. This happens at every plate of the column as shown in Fig. 4.13.4. As the liquid moves down the column, it is being heated; this heating vaporizes the more volatile constituent preferentially, so that the liquid becomes increasing enriched in the less volatile component as it moves downward from one plate to another.

If sufficient number of plates are used, it is possible to separate the two constituents of a binary liquid mixture; the more volatile constituent in the vapour form is collected from the top of the distilling column and that of lesser volatile constituent from the bottom of the column. The vapour from the top of the column is fed into a condenser where it is liquefied. Part of this liquid is drawn off and the rest is returned to the column in order to maintain the stock of essentially pure distillate on the upper plates. In order to make the separation continuous, the preheated liquid mixture is introduced somewhere within the column as shown in Fig. 4.13.3.